- Recap: Lecture 2: 24<sup>th</sup> July 2015, 1530-1655 hrs.
  - Applications of gas turbine engines
  - Review of thermodynamics concepts
    - Energy, Enthalpy, Entropy
    - *T-s* diagram
    - Isentropic processes
    - *Tds* equations

# Energy analysis of steady flow systems

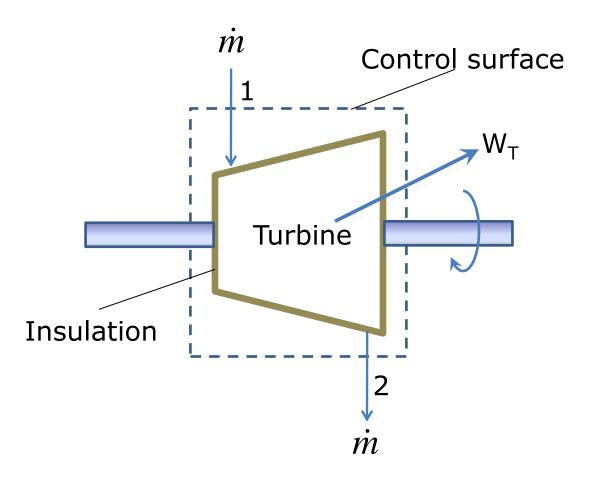
For single entry and exit devices,

$$\dot{Q} - \dot{W} = \dot{m} \left[ h_2 - h_1 + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1) \right]$$

or per unit mass,

$$\dot{q} - \dot{w} = h_2 - h_1 + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)$$

#### **Turbines and compressors**



#### **Turbines and compressors**

 For a turbine for eg., the energy equation would be:

$$\dot{m}(h_{1} + \frac{V_{1}^{2}}{2} + gz_{1}) = \dot{W}_{out} + \dot{m}(h_{2} + \frac{V_{2}^{2}}{2} + gz_{2})$$
  
If KE and PE are negligible,  
 $\dot{W}_{out} = \dot{m}(h_{1} - h_{2})$ 

- Enthalpy represents the total energy of a fluid in the absence of potential and kinetic energies.
- For high speed flows, though potential energy may be negligible, but not kinetic energy.
- Combination of enthalpy and KE is called stagnation enthalpy (or total enthalpy)

$$h_0 = h + V^2/2$$
 (kJ/kg)

Stagnation enthalpy Static enthalpy Kinetic energy

- Consider a steady flow through a duct (no shaft work, heat transfer etc.).
- The steady flow energy equation for this is:  $h_1 + V_1^2/2 = h_2 + V_2^2/2$ or,  $h_{01} = h_{02}$
- That is in the absence of any heat and work interactions, the stagnation enthalpy remains a constant during a steady flow process.

• If the fluid were brought to rest at state 2,

 $h_1 + V_1^2/2 = h_2 = h_{02}$ 

- The stagnation enthalpy represents the enthalpy of a fluid when it is brought to rest adiabatically.
- During a stagnation process, the kinetic energy of a fluid is converted to enthalpy (internal energy + flow energy), which results in an increase in the fluid temperature and pressure.

• When the fluid is approximated as an ideal gas with constant specific heats,

$$c_p T_0 = c_p T + V^2/2$$
  
or,  $T_0 = T + V^2/2c_p$ 

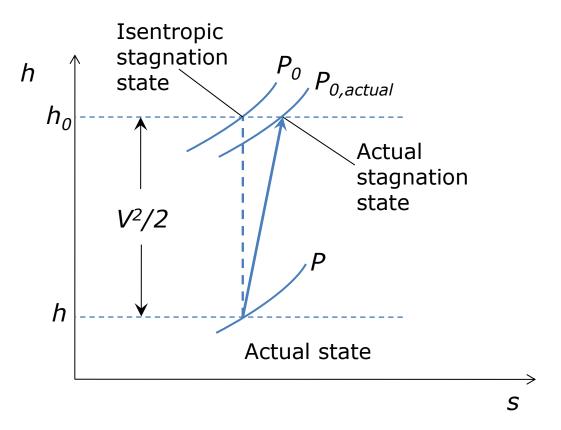
- *T<sub>0</sub>* is called the stagnation temperature and represents the temperature an ideal gas attains when it is brought to rest adiabatically.
- The term  $V^2/2c_p$  corresponds to the temperature rise during such a process and is called the dynamic temperature.

- The pressure a fluid attains when brought to rest isentropically is called the stagnation pressure,  $P_0$ .
- For ideal gases, from isentropic relations,

$$\frac{P_0}{P} = \left(\frac{T_0}{T}\right)^{\gamma/(\gamma-1)}$$

Similarly, for density wehave,

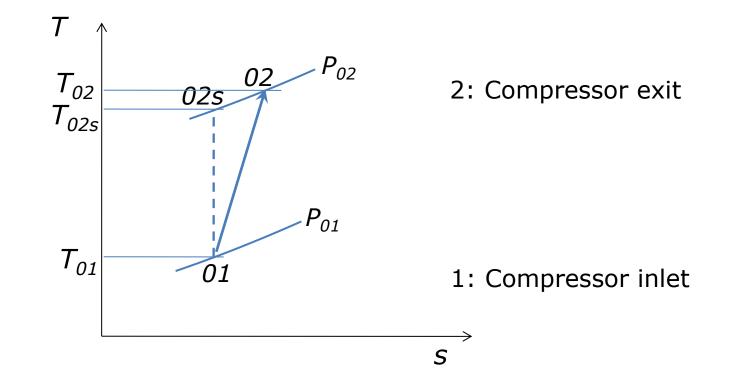
$$\frac{\rho_0}{\rho} = \left(\frac{T_0}{T}\right)^{1/(\gamma-1)}$$



The actual state, actual stagnation state, and isentropic stagnation state of a fluid on an *h-s* diagram.

- Compressors are to a high degree of approximation, adiabatic.
- Compressor performance can be evaluated using the isentropic efficiency,  $\eta_c$

 $\eta_{C} = \frac{\text{Ideal work of compression for given pressure ratio}}{\text{Actual work of compression for given pressure ratio}}$  $= \frac{w_{ci}}{w_{c}} = \frac{h_{02s} - h_{01}}{h_{02} - h_{01}}$ 



#### Actual and ideal compression processes

$$\eta_{C} = \frac{h_{02s} - h_{01}}{h_{02} - h_{01}} \cong \frac{T_{02s} - T_{01}}{T_{02} - T_{01}}$$
$$= \frac{T_{02s} / T_{01} - 1}{T_{02} / T_{01} - 1} = \frac{\left(P_{02} / P_{01}\right)^{(\gamma - 1)/\gamma} - 1}{\tau_{C} - 1}$$
$$= \frac{\left(\pi_{C}\right)^{(\gamma - 1)/\gamma} - 1}{\tau_{C} - 1}$$

 The isentropic efficiency is thus a function of the total pressure ratio and the total temperature ratio.

- Besides isentropic efficiency, there are other efficiency definitions, stage efficiency and polytropic efficiency that are used in assessing the performance of multistage compressors.
- Stage efficiency will be discussed in detail during later lectures
- The three efficiency terms can be related to one another.

• The polytropic efficiency,  $\eta_{poly}$ , is defined as  $\eta_{poly} = \frac{\text{Ideal work of compression for a differential pressure change}}{\text{Actual work of compression for a differential pressure change}}$ 

$$=\frac{dw_s}{dw}=\frac{dh_{0s}}{dh_0}=\frac{dT_{0s}}{dT_0}$$

For an ideal compressor, the isentropic relation gives,

$$T_{0s} = P_0^{(\gamma-1)/\gamma} \times \text{constant.}$$
  
And,  $dT_{0s} = T_0 \left[ \left( \frac{P_0 + dP_0}{P_0} \right)^{(\gamma-1)/\gamma} - 1 \right]$ 

Using binomial expansion for  $dP_0 / P_0 \ll 1$ ,

$$\left(1 + \frac{dP_0}{P_0}\right)^{(\gamma - 1)/\gamma} = 1 + \frac{\gamma - 1}{\gamma} \frac{dP_0}{P_0}$$

Therefore, 
$$\frac{dT_{0s}}{T_0} = \frac{\gamma - 1}{\gamma} \frac{dP_0}{P_0}$$
  
 $\eta_{poly} = \frac{dT_{0s}}{dT_0} = \frac{dT_{0s} / T_0}{dT_0 / T_0} = \frac{\gamma - 1}{\gamma} \frac{dP_0 / P_0}{dT_0 / T_0}$ 

Rewriting the above equation,

$$\frac{dT_0}{T_0} = \frac{\gamma - 1}{\gamma \eta_{poly}} \frac{dP_0}{P_0}$$

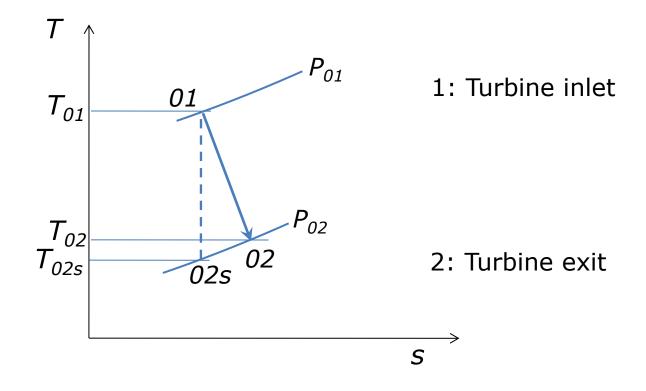
Integrating between states 01 and 02,

$$T_{02} / T_{01} = (P_{02} / P_{01})^{(\gamma - 1)/(\gamma \eta_{poly})}$$
  
or,  $\eta_C = \frac{(\pi_C)^{(\gamma - 1)/\gamma} - 1}{\tau_C - 1} = \frac{(\pi_C)^{(\gamma - 1)/\gamma} - 1}{\pi_C^{(\gamma - 1)/(\gamma \eta_{poly})} - 1}$ 

The above equation relates the isentropic efficiency with the pressure ratio assuming a constant polytropic efficiency.

- The flow in a turbine is also assumed to be adiabatic, though in actual engines there could be turbine blade cooling.
- Isentropic efficiency of the turbine is defined in a manner similar to that of the compressor.

 $\eta_t = \frac{\text{Actual work of expansion for given pressure ratio}}{\text{Ideal work of expansion for given pressure ratio}}$  $= \frac{w_t}{w_{ts}} = \frac{h_{01} - h_{02}}{h_{01} - h_{02s}} = \frac{1 - \tau_t}{1 - \pi_t^{(\gamma - 1)/\gamma}}$ 



#### Actual and ideal turbine processes

• The polytropic efficiency,  $\eta_{poly}$ , is defined as

 $\eta_{poly} = \frac{\text{Actual turbine work for a differential pressure change}}{\text{Ideal turbine work for a differential pressure change}}$ 

$$=\frac{dw}{dw_s}=\frac{dh_0}{dh_{0s}}=\frac{dT_0}{dT_{0s}}$$

For an ideal turbine, the isentropic relation gives,

$$T_{0s} = P_0^{(\gamma - 1)/\gamma} \times \text{constant. Therefore,}$$
  

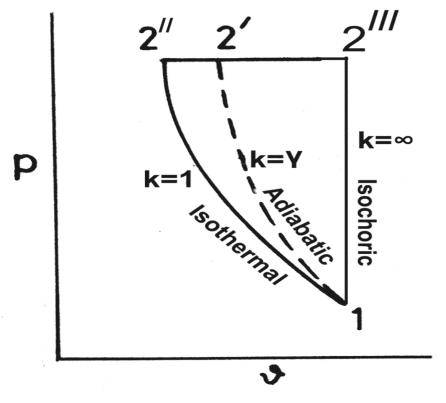
$$\frac{dT_{0s}}{T_0} = \frac{\gamma - 1}{\gamma} \frac{dP_0}{P_0}$$
  

$$\eta_{poly} = \frac{dT_0}{dT_{0s}} = \frac{dT_0 / T_0}{dT_{0s} / T_0} = \frac{dT_0 / T_0}{[(\gamma - 1) / \gamma] dP_0 / P_0}$$

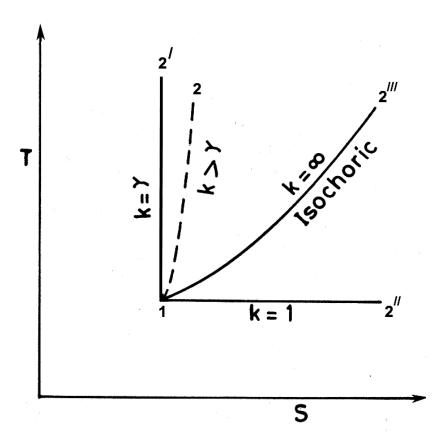
Integrating between states 01 and 02,  $\pi_{t} = \tau_{t}^{\gamma/[(\gamma-1)\eta_{poly}]}$   $or, \eta_{t} = \frac{1 - \tau_{t}}{1 - \tau_{t}^{1/\eta_{poly}}} = \frac{1 - (\pi_{t})^{(\gamma-1)\eta_{poly}/\gamma}}{1 - (\pi_{t})^{(\gamma-1)/\gamma}}$ 

The above equation relates the isentropic efficiency with the pressure ratio assuming a constant polytropic efficiency.

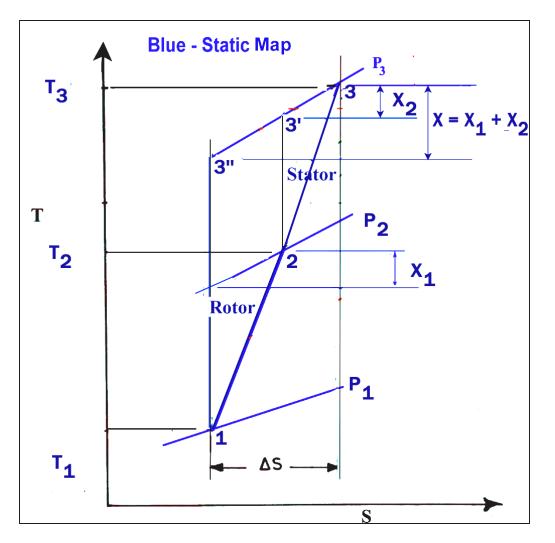
- Simplified aero-thermodynamic analysis
  - Optimised cycle design to precede the detailed component design
  - Prediction of work requirements
  - Efficiency of the compressor
  - Enables faster design modifications



- (i) Adiabatic (process  $1-2^{\prime}$ ),  $Pv^{\gamma}=c$
- (ii) Isothermal process (1-2"), Pv=c
- (iii) Isochoric (Process 1-2<sup>""</sup>), Pv = c

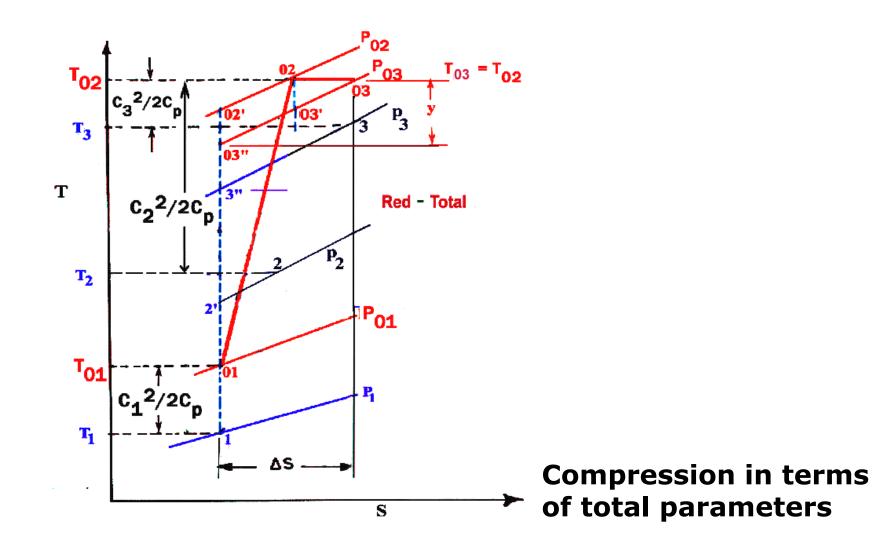


- i) Isentropic process (1-2')
- ii) Polytropic process (1-2)
- iii) Isothermal process (1-2")
- iv) Isochoric Process (1-2<sup>""</sup>)



 $X_1$ ,  $X_2$  are the losses in the rotor and the stator respectively

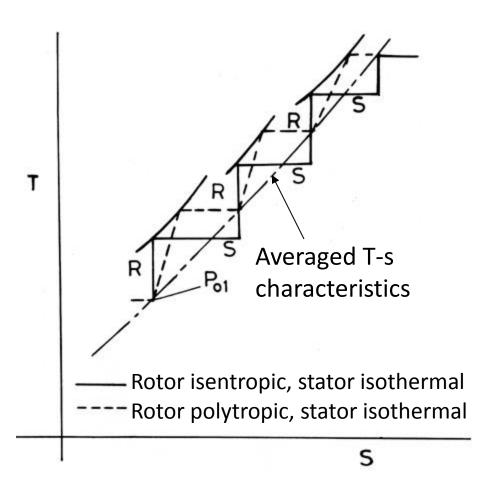
**Compression in terms** of static parameters



#### **Basic operation of axial compressors**

- Axial flow compressors usually consists of a series of stages.
- Each stage comprises of a row of rotor blades followed by a row of stator blades.
- The working fluid is initially accelerated by the rotor blades and then decelerated in the stator passages.
- In the stator, the kinetic energy transferred in the rotor is converted to static pressure.
- This process is repeated in several stages to yield the necessary overall pressure ratio.

#### Thermodynamics of multi-stage compressors



- The flow at the rotor exit with high kinetic energy is still to be converted to static pressure through diffusion.
- The exit kinetic energy of a compressor is of the same order as the entry kinetic energy and the entire work input is expected to be converted to pressure.